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THERMAL CHARACTERISTICS OF A PEBBLE BED HEATER*

Nisiki Hayashi**

ABSTRACT

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The heat transfer between pebbles contained in a circular tube and the fluid moving through it are considered. Neglecting the effect of the heat capacity of the wall, several analyses are made for the following cases: (1) the initial pebble temperature is equal to that of the fluid and is uniform, (2) the thermal capacity per unit volume of fluid is far less than that of the pebbles, and the initial pebble temperature is a linear function of $e^{-c\xi}$, where c is a constant and ξ is a nondimensional axial distance. Numerical calculations were performed for two pebble-bed heaters by means of an electronic digital computer.

Author

1. Introduction

/1***

In supersonic wind tunnels, the air temperature of the measurement section becomes very low because of its adiabatic expansion in the accelera-

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*** Note: Numbers in the margin indicate pagination in the original foreign text.

ting range. Therefore, the air must be pre-heated to raise the stagnation temperature. Generally, the following three methods are used for this purpose:

- (1) A method utilizing a metal electric heater, or a heat reservoir type heat exchanger;
- (2) A method utilizing a non-metal heat reservoir type heat exchanger;
- (3) A method utilizing an electric arc.

The contamination of fluid flow is unavoidable in the third method because of the melting electrodes, and the maximum operating temperature is too low in the first method. Therefore, the second method is to be utilized for the low temperature wind tunnel currently being planned. In this method, pebbles of material such as alumina are placed into a cylindrical container and heated by forcing hot air through it. The air to be used in the wind tunnel is pre-heated by exposing it to these pebbles. For the temperature characteristics of this air heater, an analysis of its pre-heating phase has been made in the past (Ref. 1). For the most important heat transfer characteristics during the air heating phase, however, no detailed studies have been made. This report attempts to make a detailed analysis of the thermal characteristics of this type of air heater.

2. Notation

/2

A	Non-dimensional constant	
B	Non-dimensional constant	
c	Non-dimensional constant	
C	Heat capacity of a unit volume of pebbles in the heat exchanger	kcal/m ³ °C
c _p	Constant pressure specific heat of the fluid	kcal/kg°C

$$f = (t_0 - t_i) / (T_h - t_i)$$

$G = \rho V$	Flow quantity	$\text{kg/m}^2 \text{ sec}$
h	Heat conductivity between pebbles and fluid	$\text{kcal/sec m}^{20}\text{C}$
I_0	0th degree Bessel function of the first kind	
$K = (T_i - t_i) / (T_h - t_i)$	Non-dimensional constant	
l	Length of heater	m
$\mathcal{L} ()$	Laplace transform of ()	
p	Variable of Laplace transform	
s	Heat conductivity of pebbles of unit volume	$\text{m}^2/\text{m}^3 = \text{m}^{-1}$
S	Cross sectional area of heat exchanger	m^2
s_0	Area of heat loss surface per unit volume of the heat exchanger	$\text{m}^2/\text{m}^3 = \text{m}^{-1}$
T	Fluid temperature	$^{\circ}\text{C}$
T_h	Entrance temperature of heating fluid	$^{\circ}\text{C}$
T_i	Entrance temperature of cooling fluid	$^{\circ}\text{C}$
t	Temperature of pebbles	$^{\circ}\text{C}$
t_0	Initial temperature of pebbles	$^{\circ}\text{C}$
t_s	Environmental temperature	$^{\circ}\text{C}$
U_0	Heat conductivity of environment	$\text{kcal/sec m}^{20}\text{C}$
V	Fluid flow velocity	m/sec
x	Distance along the axis of the heat exchanger in the direction of the flow	m

$\alpha = s_0 U_0 / sh$ Non-dimensional heat conductivity ratio

/3

$\beta = \alpha + 1$

$\gamma = \alpha / \beta$

$\gamma_1 = (\alpha - c) / (\beta - c)$

$\delta = (t - t_s) / (T_h - t_s)$

$\bar{\delta} = \mathcal{L}(\delta)$

$\eta = sh\tau / C$ Non-dimensional time

$\theta = (T - t_s) / (T_h - t_s)$

$\bar{\theta} = \mathcal{L}(\theta)$

$\xi = shx / Gc_p$ Non-dimensional distance

$\xi_1 = shl / Gc_p$ Non-dimensional length of heater

ρ Density of fluid kg/m^3

τ Time sec

$\psi = c_p \rho / C$ Non-dimensional heat capacity ratio

$\Psi = e^{-t-\gamma} I_0(2\sqrt{\xi\eta})$

3. Basic Equations

The case in which the pebbles are filled evenly in a cylinder of constant cross sectional area is theoretically considered, assuming the following conditions:

- (1) Temperature is affected only by time, the flow direction, and distance;
- (2) Heat conductivity of the fluid and pebbles are negligible;
- (3) The fluid flow velocity is even and constant;
- (4) The edge effect is negligible;
- (5) The heat conductivities h and U_0 are constant;
- (6) Heat transfer by radiation is negligible;
- (7) Material property constants are independent of the temperature.

/4

The heat lost from the fluid is gained by the pebbles and the environment. Therefore, the following equation can be written (Refer to Fig. 1):

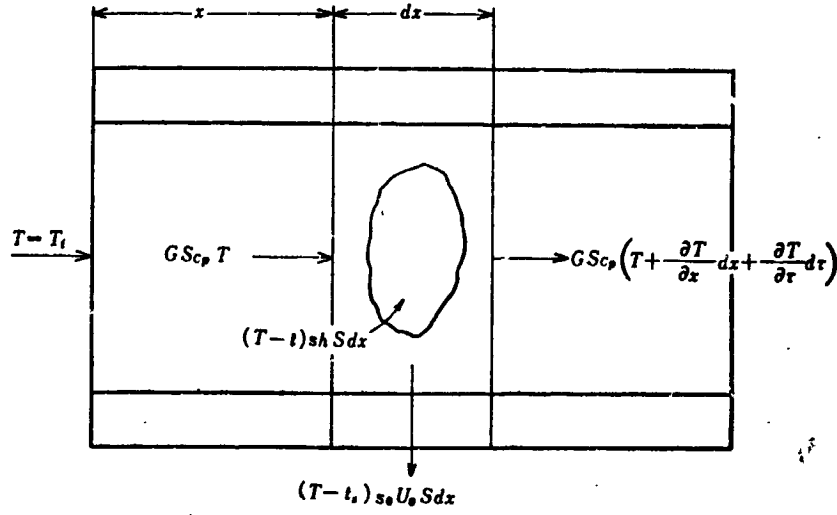


Fig. 1

$$-GSc_p \left(\frac{\partial T}{\partial x} dx + \frac{\partial T}{\partial \tau} d\tau \right) = \{ (T-t)sh + (T-t_s)s_0U_0 \} Sdx. \quad (1)$$

The relationship between the temperature increase of the pebbles and the heat gained by the pebbles can be expressed as follows (Ref. 1):

$$C \frac{\partial t}{\partial \tau} Sdx = (T-t)shSdx \quad (2)$$

Using the non-dimensional variables, we have

$$\xi = \frac{shx}{Gc_p}, \quad \eta = \frac{sh\tau}{C}, \quad \theta = \frac{T-t_s}{T_h-t_s}, \quad \delta = \frac{t-t_s}{T_h-t_s},$$

and the non-dimensional constants,

$$\psi = \frac{\rho c_p}{C}, \quad \alpha = \frac{s_0U_0}{sh}, \quad \beta = \alpha + 1$$

and if the relationship

$$d\tau = \frac{dx}{V} = \frac{\rho dx}{G}$$

is used, equation (1) becomes

$$\frac{\partial \theta}{\partial \xi} + \psi \frac{\partial \theta}{\partial \eta} = \delta - \beta \theta, \quad (3)$$

and equation (2) becomes

$$\frac{\partial \delta}{\partial \eta} = \theta - \delta \quad (4)$$

4. Heating and Cooling Characteristics at Uniform Temperatures

The case in which the initial temperature of the pebbles and that of the air are uniform and equal ($t_0 = T_0$) is considered in this section. In this case, if it is assumed that

$$A = \frac{t_0 - t_s}{T_h - t_s} = \frac{T_0 - t_s}{T_h - t_s}$$

the initial conditions can be given by the following,

$$\delta(\xi, 0) = A, \quad \theta(\xi, 0) = A \quad (5)$$

And if it is assumed that

$$K = \frac{T_i - t_s}{T_h - t_s}$$

the boundary conditions can be given as follows:

/5

$$\theta(0, \eta) = K \quad (6)$$

where $K = 1$ when heating the pebbles, and $T_i = t_s$ when cooling the pebbles.

Therefore, $K=0$.

Applying the Laplace transform to equation (3), and substituting the relationship shown in equation (5), the following can be obtained

$$\frac{d\bar{\theta}}{d\xi} + \psi(p\bar{\theta} - A) = \bar{\delta} - \beta\bar{\theta} \quad (7)$$

where, $\bar{\theta} = \mathcal{L}(\theta)$, $\bar{\delta} = \mathcal{L}(\delta)$. Also, from equations (4) and (5), the following can be obtained

$$\bar{\delta} = \frac{\bar{\theta}}{p+1} + \frac{A}{p+1} \quad (8)$$

and from equation (6), the following can be obtained

$$\bar{\theta}(0) = \frac{K}{p} \quad (9)$$

Substituting equation (8) into equation (7), we obtain the following :

$$\frac{d\bar{\theta}}{d\xi} + \left(\beta + \psi p - \frac{1}{p+1} \right) \bar{\theta} = \frac{A}{p+1} + \psi A. \quad (10)$$

The solution to equation (10) that satisfies equation (9) is as follows

$$\begin{aligned} \bar{\theta} = & \frac{K}{p} \exp \left\{ - \left(\beta + \psi p - \frac{1}{p+1} \right) \xi \right\} \\ & + \frac{A(1+\psi+\psi p)}{\psi p^2 + (\beta + \psi)p + \alpha} \left[1 - \exp \left\{ - \left(\beta + \psi p - \frac{1}{p+1} \right) \xi \right\} \right] \end{aligned} \quad (11)$$

From equation (8), the following can be obtained

$$\begin{aligned} \bar{\delta} = & A \frac{\psi p + \beta + \psi}{\psi p^2 + (\beta + \psi)p + \alpha} \\ & + \left\{ \frac{K}{p(p+1)} + \frac{A}{p+1} - A \frac{\psi p + \beta + \psi}{\psi p^2 + (\beta + \psi)p + \alpha} \right\} \exp \left\{ - \left(\beta + \psi p - \frac{1}{p+1} \right) \xi \right\} \end{aligned}$$

In this section, the case in which $\psi > 0$ will be considered. (The case in which $\psi = 0$ is considered is in the next section.)

Since,

$$D^2 = 1 + \frac{4-2\beta}{\psi} + \frac{\beta^2}{\psi^2} = \frac{4}{\psi} + \left(1 - \frac{\beta}{\psi} \right)^2 > 0$$

if it is assumed that

$$m = \frac{1}{2} \left(-1 - \frac{\beta}{\psi} + D \right), \quad n = -\frac{1}{2} \left(1 + \frac{\beta}{\psi} + D \right), \quad q = \frac{(\beta/\psi) + 1}{D}$$

then,

$$\frac{\psi p + \beta + \psi}{\psi p^2 + (\beta + \psi)p + \alpha} = \frac{(\beta/\psi) + 1 + p}{(p-m)(p-n)} = \frac{1}{2} \frac{1+q}{p-m} + \frac{1}{2} \frac{1-q}{p-n}.$$

Therefore,

$$\begin{aligned} \bar{\delta} = & \frac{A}{2} \left(\frac{1+q}{p-m} + \frac{1-q}{p-n} \right) \\ & + \left\{ \frac{K}{p(p+1)} + \frac{A}{p+1} - \frac{A}{2} \frac{1+q}{p-m} - \frac{A}{2} \frac{1-q}{p-n} \right\} e^{-\beta \xi} \exp \left\{ \left(\frac{1}{p+1} - \psi p \right) \xi \right\}. \end{aligned}$$

TABLE 1
LAPLACE TRANSFORM TABLE

/6

1 番 号	$F(p) \equiv \mathcal{L}[f(\eta)]$	$f(\eta)$	2 註
1	$\frac{1}{p+m}$	$e^{-m\eta}$	文献 2 p. 229 3
2	$\frac{1}{p-m} \exp \left\{ \left(\frac{1}{1+p} - \phi p \right) \xi \right\}$	$\begin{cases} 0 & (0 < \eta < \phi \xi) \\ (1+m)e^{m(\eta-\phi\xi)} \int_0^{\eta-\phi\xi} e^{-(1+m)\eta} I_0(2\sqrt{\xi\eta}) d\eta \\ + e^{\phi\xi-\eta} I_0[2\sqrt{\xi(\eta-\phi\xi)}] & (\phi\xi < \eta) \end{cases}$	付 録 4
3	$\frac{1}{p(p+1)} \exp \left\{ \left(\frac{1}{1+p} - \phi p \right) \xi \right\}$	$\begin{cases} 0 & (0 < \eta < \phi \xi) \\ \int_0^{\eta-\phi\xi} e^{-\eta} I_0(2\sqrt{\xi\eta}) d\eta & (\phi\xi < \eta) \end{cases}$	付 録 4

1 - No.; 2 - Remarks; 3 - Ref. 2, p. 229; 4 - Appendix

From the Laplace transform shown in Table 1, $\Psi = e^{-\xi-\eta} I_0(2\sqrt{\xi\eta})$.

Then,

$$\left. \begin{aligned} \partial &= \frac{A}{2} \{ (1+q)e^{m\eta} + (1-q)e^{n\eta} \}, & (0 < \eta < \phi\xi) \\ \partial &= \frac{A}{2} \{ (1+q)e^{m\eta} + (1-q)e^{n\eta} \} + Ke^{-\phi\xi} \int_0^{\eta-\phi\xi} \Psi d\eta \\ &\quad - \frac{A}{2} (1+q)(1+m)e^{-(m\phi\xi + m\eta)} \int_0^{\eta-\phi\xi} e^{-m\eta} \Psi d\eta \\ &\quad - \frac{A}{2} (1-q)(1+n)e^{-(n\phi\xi + n\eta)} \int_0^{\eta-\phi\xi} e^{-n\eta} \Psi d\eta. & (\phi\xi < \eta) \end{aligned} \right\} \quad (12)$$

Similarly, if

$$Q = \left(\frac{2-\beta}{\phi} + 1 \right) / D$$

then,

$$\bar{\partial} = \frac{A}{2} \left(\frac{1+Q}{p-m} + \frac{1-Q}{p-n} \right) + \left(\frac{K}{p} - \frac{A}{2} \frac{1+Q}{p-m} - \frac{A}{2} \frac{1-Q}{p-n} \right) e^{-\mu\xi} \exp \left\{ \left(\frac{1}{p+1} - \phi p \right) \xi \right\}$$

Therefore,

17

$$\left. \begin{aligned}
 \theta &= \frac{A}{2} \{ (1+Q)e^{m\eta} + (1-Q)e^{n\eta} \}, & (0 < \eta < \psi\xi) \\
 \theta &= \frac{A}{2} \{ (1+Q)e^{m\eta} + (1-Q)e^{n\eta} \} \\
 &+ (K-A)e^{-(\beta-\psi)\xi-\eta} I_0[2\sqrt{\xi(\eta-\psi\xi)}] + Ke^{-\alpha\xi} \int_0^{\eta-\psi\xi} \Psi d\eta \\
 &- \frac{A}{2} (1+Q)(1+m)e^{-(\alpha+m\phi)\xi+m\eta} \int_0^{\eta-\psi\xi} e^{-m\eta} \Psi d\eta \\
 &- \frac{A}{2} (1-Q)(1+n)e^{-(\alpha+n\phi)\xi+n\eta} \int_0^{\eta-\psi\xi} e^{-n\eta} \Psi d\eta, & (\psi\xi < \eta)
 \end{aligned} \right\} \quad (13)$$

When, $\psi < 1$

$$m = -\gamma + \frac{\gamma}{\beta^2} \psi + O(\psi^2), \quad n = -\frac{\beta}{\psi} - \frac{1}{\beta} + O(\psi), \quad q = 1 + \frac{2\gamma}{\beta} \psi + O(\psi^2)$$

Therefore, if δ , when $\psi=0$, is δ_0 , then we have

$$\left. \begin{aligned}
 \delta &= \delta_0 \left\{ 1 + \frac{\gamma}{\beta} \left(1 + \frac{n}{\beta} \right) \psi \right\}, & (0 < \eta < \psi\xi) \\
 \delta &= \delta_0 + \left[A \frac{\gamma}{\beta} e^{-r\eta} \left\{ 1 + \frac{n}{\beta} - e^{-\alpha\xi} \left(\frac{2}{\beta} + \xi + \frac{n}{\beta^2} \right) \int_0^\eta e^{r\eta} \Psi d\eta \right. \right. \\
 &\quad \left. \left. + e^{-\alpha\xi} \frac{1}{\beta^2} \int_0^\eta e^{r\eta} \Psi \eta d\eta \right\} + \xi \Psi e^{-\alpha\xi} \left(\frac{A}{\beta} - K \right) \right] \psi, & (\psi\xi < \eta)
 \end{aligned} \right\} \quad (14)$$

where,

$$\begin{aligned}
 \delta_0 &= Ae^{-r\eta}, & (0 < \eta < \psi\xi) \\
 \delta_0 &= Ae^{-r\eta} + Ke^{-\alpha\xi} \int_0^\eta \Psi d\eta - \frac{A}{\beta} e^{-\alpha\xi-r\eta} \int_0^\eta e^{r\eta} \Psi d\eta & (\psi\xi < \eta)
 \end{aligned}$$

which is a solution already known (Ref. 1).

When the pebbles, which are sufficiently cooled initially ($A = 0$), are heated ($K = 1$), the second equation shown in equation (14) becomes as follows:

$$\delta = \delta_0 - \psi\xi\Psi e^{-\alpha\xi} = e^{-\alpha\xi} \left(\int_0^\eta \Psi d\eta - \psi\xi\Psi \right) \quad (\psi\xi < \eta) \quad (15)$$

5. Heating and Cooling Characteristics of a General Case

The case in which the initial temperature of the pebbles and that of the air are unspecified will be considered in this section. For this condition,

assumption $\psi=0$ will be introduced. If it is assumed that,

$$f(\xi) = \frac{t_0 - t_i}{T_a - T_i}$$

the initial conditions can be given as follows. /8

$$\delta(\xi, 0) = f(\xi)$$

The boundary conditions can be given, similarly to the previous section, as follows:

$$\theta(0, \eta) = K$$

Allowing $\psi=0$, and $A=f$, the following can be obtained from equation (10):

$$\frac{d\bar{\theta}}{d\xi} + \left(\beta - \frac{1}{p+1}\right)\bar{\theta} = \frac{f}{p+1}.$$

The solution to this equation which satisfies equation (9) is as follows,

$$\bar{\theta} = \left[\frac{K}{p} + \frac{1}{p+1} \int_0^\xi f \exp\left\{\left(\beta - \frac{1}{p+1}\right)\xi\right\} d\xi \right] \exp\left\{-\left(\beta - \frac{1}{p+1}\right)\xi\right\}$$

Allowing $A=f$, the following can be obtained from equation (8),

$$\begin{aligned} \bar{\theta} = & \frac{f}{p+1} + \frac{K}{p(p+1)} \exp\left\{-\left(\beta - \frac{1}{p+1}\right)\xi\right\} \\ & + \frac{1}{(p+1)^2} \left[\exp\left\{-\left(\beta - \frac{1}{p+1}\right)\xi\right\} \right] \int_0^\xi f \exp\left\{\left(\beta - \frac{1}{p+1}\right)\xi\right\} d\xi \end{aligned}$$

In the subsequent discussion, the case in which the following condition is true will be considered.

$$I = A - B e^{-c\xi} \tag{16}$$

Since,

$$\begin{aligned} \int_0^\xi f \exp\left\{\left(\beta - \frac{1}{p+1}\right)\xi\right\} d\xi = & \frac{A(p+1)}{\beta p + \alpha} \left[\exp\left\{\left(\beta - \frac{1}{p+1}\right)\xi\right\} - 1 \right] \\ & - \frac{B(p+1)}{(\beta - c)p + \alpha - c} \left[\exp\left\{\left(\beta - c - \frac{1}{p+1}\right)\xi\right\} - 1 \right] \end{aligned}$$

if the condition of $\gamma = \alpha/\beta$, $\gamma_1 = (\alpha - c)/(\beta - c)$ is used, the following can be obtained

$$\begin{aligned}
\bar{\delta} &= \frac{A}{p+r} - \frac{Be^{-ct}}{p+r_1} + \frac{Ke^{-\mu t}}{p(p+1)} \exp\left(\frac{\xi}{p+1}\right) \\
&\quad - \frac{A(1-r)e^{-\mu t}}{(p+r)(p+1)} \exp\left(\frac{\xi}{p+1}\right) + \frac{B(1-r_1)e^{-\mu t}}{(p+r_1)(p+1)} \exp\left(\frac{\xi}{p+1}\right), \\
\bar{\theta} &= \frac{A}{\beta} \frac{1}{p+r} - \frac{Be^{-ct}}{\beta-c} \frac{1}{p+r_1} + Ke^{-\mu t} \left\{ \frac{1}{p(p+1)} + \frac{1}{p+1} \right\} \exp\left(\frac{\xi}{p+1}\right) \\
&\quad - \frac{Ae^{-\mu t}}{\beta} \left\{ \frac{1-r}{(p+r)(p+1)} + \frac{1}{p+1} \right\} \exp\left(\frac{\xi}{p+1}\right) \\
&\quad + \frac{Be^{-\mu t}}{\beta-c} \left\{ \frac{1-r_1}{(p+r_1)(p+1)} + \frac{1}{p+1} \right\} \exp\left(\frac{\xi}{p+1}\right)
\end{aligned}$$

Converting it back and using relationship, $\Psi = e^{-t-\eta} I_0(2\sqrt{\xi\eta})$, the following can be obtained. /9

$$\begin{aligned}
\delta &= Ae^{-\eta} - Be^{-ct-\eta} + Ke^{-\mu t} \int_0^\eta \Psi d\eta - A(1-r)e^{-\mu t-\eta} \int_0^\eta e^{\eta} \Psi d\eta \\
&\quad + B(1-r_1)e^{-\mu t-\eta} \int_0^\eta e^{\eta} \Psi d\eta,
\end{aligned} \tag{17}$$

$$\begin{aligned}
\theta &= A(1-r)e^{-\eta} - B(1-r_1)e^{-ct-\eta} + \{K - A(1-r) + B(1-r_1)\}e^{-\mu t} \Psi \\
&\quad + Ke^{-\mu t} \int_0^\eta \Psi d\eta - A(1-r)^2 e^{-\mu t-\eta} \int_0^\eta e^{\eta} \Psi d\eta + B(1-r_1)^2 e^{-\mu t-\eta} \int_0^\eta e^{\eta} \Psi d\eta
\end{aligned} \tag{18}$$

6. Cooling at Even Temperatures

In the case where sufficient heating is performed over a prolonged period of time, and where there is no heat loss from the walls, it becomes, $t_0 = T_h$. Therefore, $f=A=1$ and $B=0$. If the entrance temperature of the cooling flow is the same as that of the surrounding environment $K = 0$, equations (17) and (18) become as follows, respectively:

$$\delta = e^{-\eta} - (1-r)e^{-\mu t-\eta} \int_0^\eta e^{\eta} \Psi d\eta, \tag{19}$$

$$\theta = (1-r) \left\{ e^{-\eta} - e^{-\mu t} \Psi - (1-r)e^{-\mu t-\eta} \int_0^\eta e^{\eta} \Psi d\eta \right\} \tag{20}$$

This result agrees with the solution already known (Ref. 1).

7. Cooling at Even Temperatures After Prolonged Heating

Considering the case where the temperature is even and equal to that of the environment, $t_0 = t_s$, the following, $f=A=B=0$, is true. Because, $K = 1$, the following equations can be obtained:

$$\delta = e^{-\alpha t} \int_0^{\eta} \Psi d\eta, \quad (21)$$

$$\theta = e^{-\alpha t} \left(\Psi + \int_0^{\eta} \Psi d\eta \right) \quad (22)$$

These results also agree with the solutions already known (Ref. 1). Now, because of the following relationship,

$$\int_0^{\infty} \Psi d\eta = e^{-t} \int_0^{\infty} e^{-\eta} I_0(2\sqrt{\xi\eta}) d\eta = 1,$$

$$\lim_{\eta \rightarrow \infty} e^{-\eta} I_0(2\sqrt{\xi\eta}) = \lim_{\tau \rightarrow \infty} e^{-\tau/4\xi} I_0(\tau) = 0$$

after sufficient prolonged heating, the following condition is true (Ref. 1)

$$\theta = \delta = e^{-\alpha t} \quad (23)$$

The case of forced air cooling beginning with this condition is to be /10 considered.

(1) Heating flow and cooling flow are flowing in the same direction.

In this case, the following relationship can be established:

$$f = \delta = e^{-\alpha t}$$

Therefore, $A=0$, $B=-1$, $c=\alpha$, $\gamma_1=0$. Thus, the following results

$$\delta = e^{-\alpha t} - (1-K) e^{-\alpha t} \int_0^{\eta} \Psi d\eta, \quad (24)$$

$$\theta = e^{-\alpha t} + (K-1) e^{-\alpha t} \left(\Psi + \int_0^{\eta} \Psi d\eta \right). \quad (25)$$

(2) Heating flow and the cooling flow are flowing in the opposite direction.

Using the length of the heater, l , the following equation, $\xi_1 = shl/Gc_p$, can be obtained. Then, because the following relationship holds

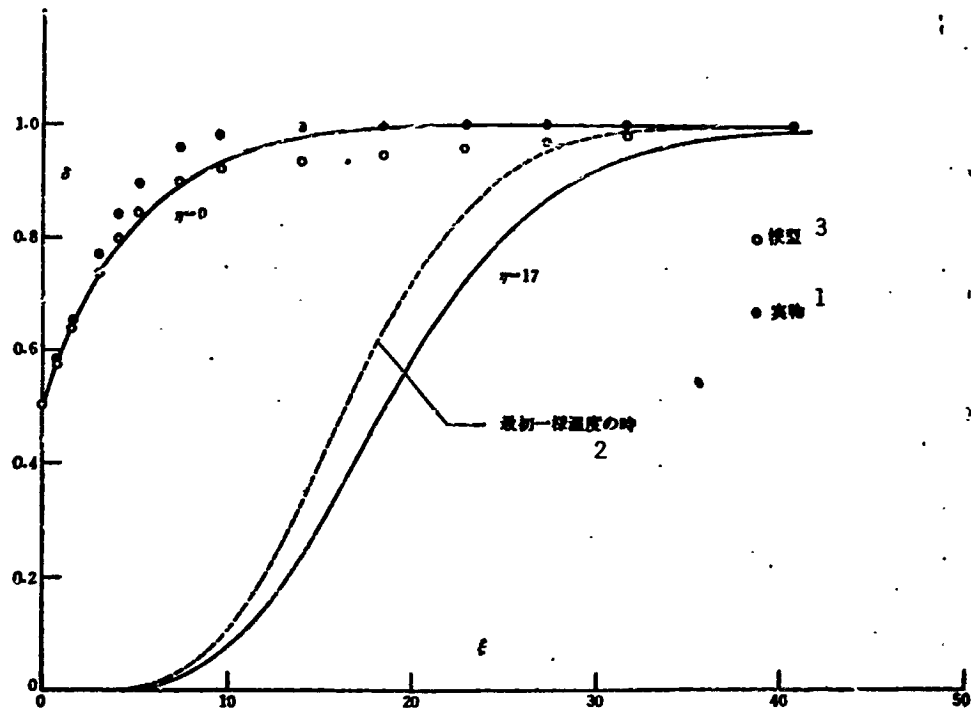


Figure 2

Cooling Characteristics (Pebble temperature)

- (1) - Actual heater; (2) - The case of uniform initial temperature;
(3) - Model.

$$j = e^{-\alpha t_1} e^{\alpha t}$$

the following can be obtained:

$$A=0, B=-e^{-\alpha t_1}, c=-\alpha, \gamma_1=2\alpha/(2\alpha+1)$$

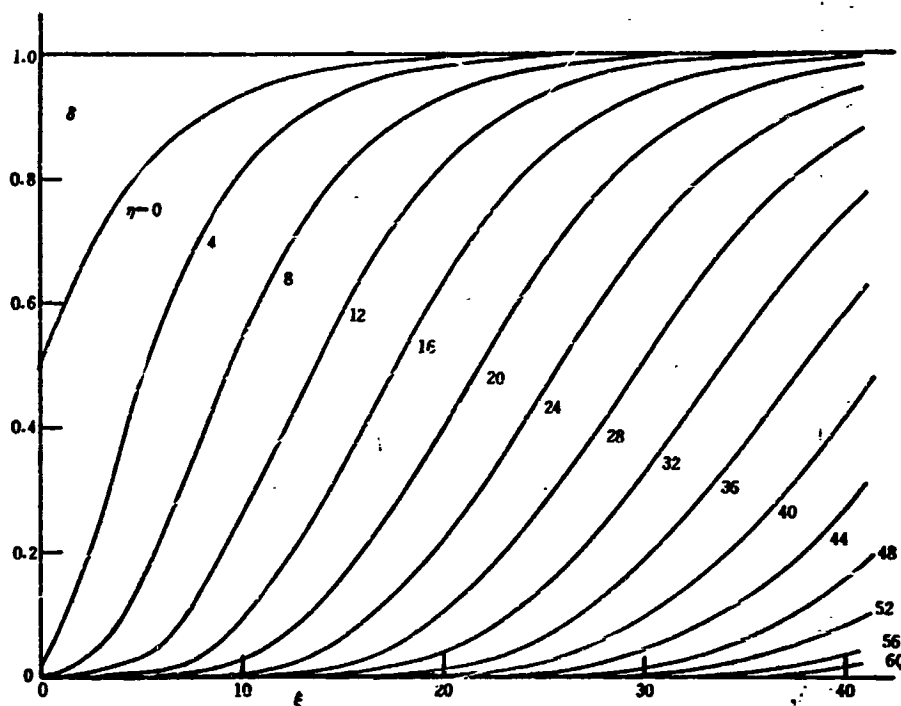
Thus,

$$\theta = e^{-\alpha t_1} e^{\alpha t - \gamma_1 t} + K e^{-\alpha t} \int_0^t \Psi d\eta - (1-\gamma_1) e^{-\alpha t_1} e^{-\alpha t - \gamma_1 t} \int_0^t e^{\gamma_1 \eta} \Psi d\eta, \quad (26)$$

$$\begin{aligned} \theta = & (1-\gamma_1) e^{-\alpha t_1} e^{\alpha t - \gamma_1 t} + \{K - (1-\gamma_1) e^{-\alpha t_1}\} e^{-\alpha t} \Psi \\ & + K e^{-\alpha t} \int_0^t \Psi d\eta - (1-\gamma_1)^2 e^{-\alpha t_1} e^{-\alpha t - \gamma_1 t} \int_0^t e^{\gamma_1 \eta} \Psi d\eta. \end{aligned} \quad (27)$$

8. Calculation Examples

As an actual calculation example, a calculation was made for the heater to be used with the super-sonic wind tunnel currently under construction,



/12

Figure 3

Cooling Characteristics (Pebble temperature)

and for this heater's preliminary experimental mockup. The constants for this case are shown in Table 2. For these values of the constants, the temperature distribution of the pebbles was calculated using equation (15) for the case in which it was heated until the value of δ reached $1/2$ at the end of heating. The results obtained are shown in Fig. 2 as \circ (for the model) and \bullet (for the actual heater). Using pebbles having this type of temperature distribution, we investigated the cooling characteristics for the case in which cooling air flowed in the opposite direction to the heating air flow. The temperature distribution was approximated by equation (16) assuming the following values:

$$A=1.0001260, \quad B=0.50012594, \quad c=0.20489647$$

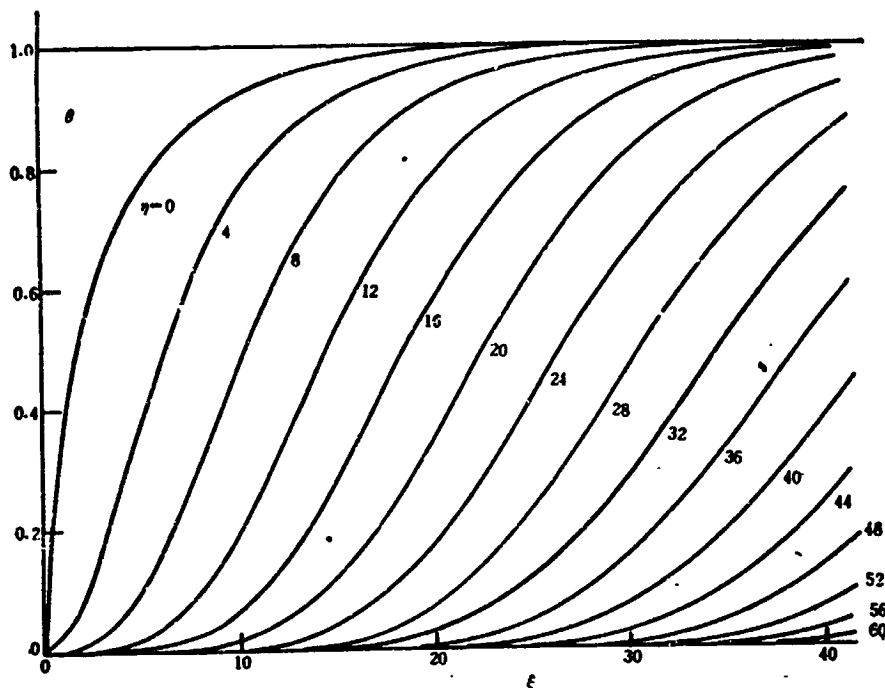


Figure 4

Cooling Characteristics (Air temperature)

This result is shown in the same figure as solid line ($\eta=0$). Using this result and setting $\gamma=K=0$, the results obtained from equation (17) are shown in the same figure as the solid line ($\eta=17$).^{*} For purposes of reference, the results of $\eta=17$ obtained from equation (19) assuming an even initial temperature, $\delta=1$, are shown by the dotted line. These results show that there is a considerable difference in the temperature distribution. Figure 3 shows the temperature distributions of the pebbles where $\eta=0(4)60$. The air temperature, θ , is shown in Fig. 4. In Fig. 5, the temperature of air flowing out of the end of the cooler is shown as a function of the non-dimensional time, η . The solid line shows the results obtained from equation (20).

^{*}The α during cooling is small as shown in Table 2, and the results differ very little even if $\gamma=0$.

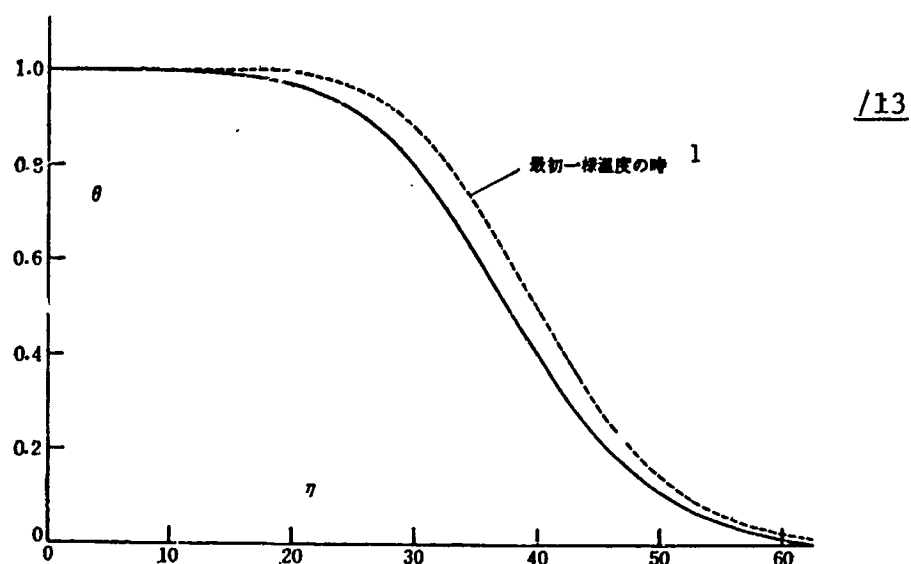


Figure 5

Exit Flow Temperature

(1) - The case of uniform initial temperature

In closing, I wish to thank Professor Isao Imai of the University of Tokyo, Aero-navigation Laboratory and Dr. Tomio Yamaguchi of the Shinmitsubishi Heavy Industry Co., Kobe Ship-yard Laboratory who gave valuable advice during this research.

TABLE 2

	$\alpha \times 10^4$	$\xi/x \text{ (m}^{-1}\text{)}$	η/t	ϕ
Heating	model 5.88 actual 1.02	92.1	141 (h ⁻¹)	0.003
Cooling	model 1.71 actual 0.297	20.22	8.09 (min ⁻¹)	0

(Basis of calculation of results shown in Table 2)

(1) s_0 If the diameter of the heat exchanger is $D(m)$, the surface area per unit length is πD , and the volume is $\pi D^2/4$. Therefore,

$$s_0 = \frac{\pi D}{\frac{\pi}{4} D^2} = \frac{4}{D}.$$

(2) s If the diameter of the pebble is d(m), and the gap factor of the filling layer is e, then,

$$s = \frac{6(1-e)}{d}.$$

For the most densely packed case, e is $1-(\pi/2\sqrt{6})=0.3587$.

(3) c_p 0.265 kcal/kg^oC.

(4) C If the apparent specific gravity of the alumina is assumed to be 3.3, and the specific heat is assumed to be 0.244 kcal/kg^oC, then,

$$C = 3300 \times 0.6413 \times 0.244 = 516.4 \text{ (kcal/m}^3 \text{ } ^\circ\text{C)}.$$

(5) G, h Heating $G = 2982 \text{ kcal/m}^2 \text{ h}$, $h = 180 \text{ kcal/m}^2 \text{ h } ^\circ\text{C}$,

Cooling $G = 46768 \text{ kg/m}^2 \text{ h}$, $h = 620 \text{ kcal/m}^2 \text{ h } ^\circ\text{C}$.

(6) U_o , D, d

	U_o (kcal/m ² h °C)	D (m)	d (m)
model	3.21	0.3	9.5×10^{-4}
actual	2.60	1.4	9.5×10^{-4}

Appendix

/14

The second and third Laplace transforms shown in Table 1 will be derived. The table of Laplace transforms used as the basis, extracted from (Ref. 2) are shown in Table 3.

(1) Derivation of second transforms

$$\frac{1}{p-m} \exp\left\{\left(\frac{1}{p+1} - \phi p\right)\xi\right\} = \frac{1}{p-m} \left\{ \exp\left(\frac{\xi}{p+1}\right) - 1 \right\} e^{-\phi \xi p} + \frac{1}{p-m} e^{-\phi \xi p}. \quad (\text{A.1})$$

Now, from 1 and 4 of Table 3, we have

$$\exp\left(\frac{\xi}{p+1}\right) - 1 = \mathcal{L}\left[e^{-\eta}\left(\frac{\xi}{\eta}\right)^{1/2} I_1(2\sqrt{\xi\eta})\right]. \quad (\text{A.2})$$

TABLE 3

LIST OF LAPLACE TRANSFORMS

No.	$F(p) \equiv \mathcal{L}[f(\eta)]$	$f(\eta)$	Pg. no. of Ref. 2
1	$F(p-A)$	$e^{A\eta} f(\eta)$	p. 129
2	$F_1(p)F_2(p)$	$\int_0^\eta f_1(z)f_2(\eta-z)dz$	p. 131
3	$\frac{1}{p-m} e^{-Ap} \quad (A>0)$	$\begin{cases} 0 & (0<\eta<A) \\ e^{m(\eta-A)} & (A<\eta) \end{cases}$	p. 242
4	$\exp\left(\frac{\xi}{p}\right)-1$	$\left(\frac{\xi}{\eta}\right)^{1/2} I_1(2\sqrt{\xi\eta})$	p. 244
5	$\frac{1}{p} \exp\left(\frac{\xi}{p}\right)$	$I_0(2\sqrt{\xi\eta})$	p. 245

and from 3 of Table 3,

$$\frac{1}{p-m} e^{-\phi\xi p} = \begin{cases} \mathcal{L}[0], & (0 < \eta < \psi\xi) \\ \mathcal{L}[e^{m(\eta-\phi\xi)}], & (\psi\xi < \eta) \end{cases} \quad (\text{A.3})$$

From these two equations and from 2 of Table 3, we have

$$\left\{ \exp\left(\frac{\xi}{p+1}\right) - 1 \right\} \frac{1}{p-m} e^{-\phi\xi p} = \mathcal{L}\left[\int_0^\eta e^{-xz} \left(\frac{\xi}{z}\right)^{1/2} I_1(2\sqrt{\xi z}) \Delta(\eta-z) dz \right],$$

where

$$\Delta(\eta-z) = \begin{cases} 0, & (\eta - \psi\xi < z) \\ e^{m(\eta-z-\phi\xi)}, & (0 < z < \eta - \psi\xi) \end{cases}$$

Therefore,

$$\frac{1}{p-m} \left\{ \exp\left(\frac{\xi}{p+1}\right) - 1 \right\} e^{-\phi\xi p} = \begin{cases} \mathcal{L}[0], & (0 < \eta < \psi\xi) \\ \mathcal{L}\left[e^{m(\eta-\phi\xi)} \int_0^{\eta-\phi\xi} e^{-(1+m)\eta} \left(\frac{\xi}{\eta}\right)^{1/2} I_1(2\sqrt{\xi\eta}) d\eta \right], & (\psi\xi < \eta) \end{cases}$$

Substituting this equation and equation (A.3) into equation (A.1),

$$\begin{aligned} & \frac{1}{p-m} \exp\left\{ \left(\frac{1}{p+1} - \psi p \right) \xi \right\} \\ &= \begin{cases} \mathcal{L}[0], & (0 < \eta < \psi\xi) \\ \mathcal{L}\left[e^{m(\eta-\phi\xi)} \left\{ 1 + \int_0^{\eta-\phi\xi} e^{-(1+m)\eta} \left(\frac{\xi}{\eta}\right)^{1/2} I_1(2\sqrt{\xi\eta}) d\eta \right\} \right], & (\psi\xi < \eta) \end{cases} \end{aligned} \quad (\text{A.4})$$

Now,

$$\begin{aligned} & \int_0^{\eta-\phi\xi} e^{-(1+m)\eta} \left(\frac{\xi}{\eta}\right)^{1/2} I_1(2\sqrt{\xi\eta}) d\eta = \int_0^{\eta-\phi\xi} e^{-(1+m)\eta} \frac{dI_0}{d\eta} d\eta \\ &= e^{(1+m)(\phi\xi-\eta)} I_0[2\sqrt{\xi(\eta-\psi\xi)}] - 1 + (1+m) \int_0^{\eta-\phi\xi} e^{-(1+m)\eta} I_0(2\sqrt{\xi\eta}) d\eta. \end{aligned}$$

Therefore, the second transform in Table 1 is derived.

(11) Derivation of third transform

From 1 and 5 of Table 3, we have

$$\frac{1}{p+1} \exp\left(\frac{\xi}{p+1}\right) = e^{-\eta} I_0(2\sqrt{\xi\eta}).$$

Therefore, using 2 of Table 3,

$$\begin{aligned} \frac{1}{p(p+1)} \exp\left\{\left(\frac{1}{p+1} - \psi p\right)\xi\right\} &= \frac{1}{p+1} \exp\left(\frac{\xi}{p+1}\right) \frac{1}{p} e^{-\psi \xi p} \\ &= \mathcal{L}\left[\int_0^\eta e^{-z} I_0(2\sqrt{\xi z}) \Delta(\eta-z) dz\right], \end{aligned}$$

where,

$$\Delta(\eta-z) = \begin{cases} 0, & (\eta - \psi\xi < z) \\ 1, & (0 < z < \eta - \psi\xi) \end{cases}$$

Therefore, the third transform in Table 3 can be derived.

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NAL TR-52

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/16

National Aerospace Laboratory

II NAL TR-52

Thermal Characteristics of a Pebble-Bed Heater

III 536.2

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621.43

The transient thermal characteristics of a heater, having pebbles evenly filled in a cylinder of constant cross sectional area, in which a fluid of different temperature flowed, were calculated assuming the following conditions. Temperature is a function of time and distance in the direction of flow only; the flow velocity is uniform and constant; the heat transfer due to heat conduction and radiation, and the edge effect are negligible; the heat conductivity is constant; and the material property constants are independent of temperature.

A detailed analysis was made for the case in which the initial temperatures of the pebbles and the fluid were equal and uniform. Also, a solution was derived for the case in which the heat capacity of the fluid is negligible compared with that of the pebbles, and the initial temperature distribution of the pebbles can be expressed as $A - Be^{-c\xi}$ (where A, B, c are constants, and ξ is non-dimensional axial distance).*

*Note: There are four identical parts of what appears to be a library index card on this page.

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